



Time Dependent Pressure Gradient Effects on Unsteady MHD Couette Flow Through a Parallel Porous Plate

E.O. Anyanwu¹, D. Raymond²

^{1,2}Federal University Wukari, Wukari, Taraba State, Nigeria

ARTICLE INFO

Published online:

31 July 2023

Corresponding Name

E.O. Anyanwu

ABSTRACT

In this paper, the unsteady MHD Couette flow through a porous medium of a viscous incompressible fluid bounded by two parallel porous plates under the influence of thermal radiation and chemical reaction is investigated. A uniform suction and injection are applied perpendicular to the plates while the fluid motion is subjected to time dependent pressure gradient. The transformed conservation equations are solved analytically subject to physically appropriate boundary conditions by using perturbation and Eigenfunction expansion techniques. The effects of some non-dimensional parameters are graphically represented and interpreted. It is observed that primary velocity is maximum when pressure gradient is time dependent as compared to when it is independent on time. Also, increase in temperature dependent pressure gradient leads to oscillation in primary velocity along distance y .

KEYWORDS: Perturbation Method, MHD, Time dependent pressure gradient, suction, Hall current, Eigenfunction expansion technique.

1. INTRODUCTION

The dynamics of fluids through porous channel has been a popular area of research regarding to numerous increasing applications in chemical, mechanical and material process engineering. Examples of such fluid includes clay coating, coal, oil slurries, shampoo, paints cosmetic products, grease, custard and physiological liquids (blood, bile, and synovial fluid). Over the years, considerable interest has been observed on the effect of MHD in viscous, incompressible, non-Newtonian fluid flow with heat transfer. These interests on non-Newtonian fluids are owed to its important applications in various branches of science, engineering and technology, particularly in chemical and nuclear industries, material processing, geophysics and bio-engineering. In view of these applications, an extensive range of mathematical models have been developed to simulate the diverse hydrodynamic behavior of these non-Newtonian fluids. However, different non-Newtonian fluid models have been presented by researchers and solved using various types of analytical and computational schemes.

Anyanwu *et al.* [1] studied the radiative effects on unsteady MHD Couette flow through a parallel plate with constant pressure gradient. Olayiwola [2] investigated the modeling and simulation of combustion fronts in porous media. Jana *et al.* [3] examined Couette flow through a porous medium in a

rotating system. In another related work, Seth *et al.* [4] studied the effects of rotation and magnetic field on unsteady Couette flow in a porous channel. Seth *et al.* [5] studied the unsteady hydromagnetic Couette flow within porous plates in a rotating system. Recently, Sharma & Yadav [6] considered Heat transfer through three dimensional Couette flow between a stationary porous plate bounded by porous medium and moving porous plates. Sharma *et al.* [7] investigated the steady laminar flow and heat transfer of a non-Newtonian fluid through a straight horizontal porous channel in the presence of heat source. Olayiwola & Ayeni [8] examined a mathematical model and simulation of In-situ combustion in porous media. In another related work, the mathematical model of solid fuel Arrhenius combustion in a fixed-bed was analyzed by Olayiwola [9]. Bhattacharyya *et al.* [10] studied analytically the solution for magnetohydrodynamic boundary layer flow of Casson fluid over a stretching/shrinking sheet with wall mass transfer. The unsteady boundary layer flow of a Casson fluid due to an impulsively started moving plate was considered by Mustafa *et al.* [11]. Recently, Mukhopadhyay *et al.* [12] investigated the steady boundary layer flow and heat transfer over a porous moving plate in the presence of thermal radiation. Makinde and Mhone [13] studied the heat transfer to MHD flow in a channel filled with porous medium. Malapati & Polarapu [14] analyzed unsteady MHD free

Time Dependent Pressure Gradient Effects on Unsteady MHD Couette Flow Through a Parallel Porous Plate

convective heat and mass transfer in a boundary layer flow past a vertical permeable plate with thermal radiation and chemical reaction. Chamkha and Ahmed [15] examined unsteady MHD heat and mass transfer by mixed convection flow in the forward stagnation region of a rotating sphere at different wall conditions. The effects of thermal radiation and magnetic field on unsteady mixed convection flow and heat transfer over a stretching in the presence of internal heat generation/absorption was studied by Elbashbeshy & Aldawody [16]. Talukdar [17] investigated the buoyancy and chemical reaction effects on MHD mixed convection heat and mass transfer in a porous medium with thermal radiation and ohmic heating. Mohammed *et al.* [18] analyzed radiation and mass transfer effects on MHD oscillatory flow in a channel filled with porous medium in the presence of chemical reaction. The aim of the research is to establish an analytical solution capable of describing the concentration, temperature and velocity in the process of MHD Couette flow through a parallel plate.

2. MATHEMATICAL FORMULATION

Following Anyanwu *et al.* [1] while they analyzed the flow under constant pressure gradient, the unsteady flow of a viscous, incompressible, non-conducting fluid through a channel with chemical reaction and thermal radiation in the

presence of magnetic field is investigated under a time/temperature dependent pressure gradient. The flow is assumed to be laminar, incompressible and flows between two infinite horizontal plates located at $y = \pm h$ which extends from $x = -\infty$ to ∞ and from $z = -\infty$ to ∞ .

The upper plate is suddenly set into motion and moves with a uniform velocity U_0 while the lower plate is kept stationary as shown in the diagram below. The upper plate is simultaneously subjected to a step change in temperature from T_1 to T_2 . The upper and lower plates are kept at two constant temperatures T_2 and T_1 respectively with $T_2 > T_1$. The fluid flows between the two plates under the influence of an exponential decaying with time pressure gradient in the x-direction which is a generalization of a constant pressure gradient. A uniform suction from above and injection from below with constant velocity V_0 which are all applied at $t = 0$. The system is subjected to a uniform magnetic field B_0 in the positive y-direction and is assumed undisturbed as the induced magnetic field is neglected by assuming a small magnetic Reynolds number. The Hall effect is considered hence which gives rise to a z-component of velocity.

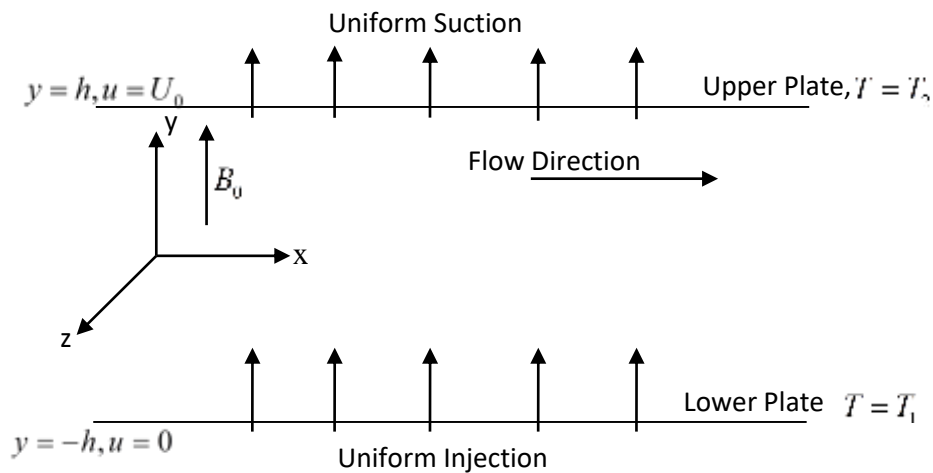


Figure 1: Schematic diagram of the problem

Based on the above assumptions,

$$v = ui + v_0j + wk \quad (1)$$

Introducing a Chapman-Rubens viscosity law, with $w = 1$ as shown in Olayiwola (2016) and using the condition at the lower plate, results in:

$$\mu = \frac{c\mu_1 T}{T_1} \quad (2)$$

Where μ_1 is the Casson coefficient of viscosity.

Thus, the two components of the governing momentum equation in dimensional form are as follows:

Time Dependent Pressure Gradient Effects on Unsteady MHD Couette Flow Through a Parallel Porous Plate

$$\rho \frac{\partial u}{\partial t} + \rho v_0 \frac{\partial u}{\partial y} = -\frac{\partial p}{\partial x} + \frac{\partial}{\partial y} \left(\mu \frac{\partial u}{\partial y} \right) - \frac{\sigma B_0^2}{(1 + BiBe)^2 + Be^2} [(1 + BiBe)u + Bew] -$$

$$\mu \frac{u}{k} + g\beta_T (T - T_1) + g\beta_C (C - C_1)$$

(3)

$$\rho \frac{\partial w}{\partial t} + \rho v_0 \frac{\partial w}{\partial y} = \frac{\partial}{\partial y} \left(\mu \frac{\partial w}{\partial y} \right) - \frac{\sigma B_0^2}{(1 + BiBe)^2 + Be^2} [(1 + BiBe)w - Beau] - \mu \frac{w}{k}$$

(4)

The energy equation in dimensional form is given as

$$\left. \begin{aligned} \rho C_p \frac{\partial T}{\partial t} + \rho C_p v_0 \frac{\partial T}{\partial y} &= \frac{1}{Pr} \frac{\partial}{\partial y} \left(\mu \frac{\partial T}{\partial y} \right) + \mu \left[\left(\frac{\partial u}{\partial y} \right)^2 + \left(\frac{\partial w}{\partial y} \right)^2 \right] + \\ &\frac{\sigma B_0^2}{(1 + BiBe)^2 + Be^2} [u^2 + w^2] - \frac{1}{\rho C_p} \frac{\partial q}{\partial y} \end{aligned} \right\} \quad (5)$$

The concentration equation in dimensional form is given as:

$$\rho \frac{\partial C}{\partial t} + \rho v_0 \frac{\partial C}{\partial y} = \frac{1}{Sc} \frac{\partial}{\partial y} \left(\mu \frac{\partial C}{\partial y} \right) + D_1 \frac{\partial^2 T}{\partial y^2} - D_2 (C_2 - C_1) \quad (6)$$

Subject to the initial and boundary conditions;

$$\left. \begin{aligned} u(y, 0) &= 0, & u(-h, t) &= 0, & u(h, t) &= U_0 \\ w(y, 0) &= U_0 y(1 - y), & w(-h, t) &= 0, & w(h, t) &= 0 \\ T(y, 0) &= 0, & T(-h, t) &= T_1, & T(h, t) &= T_2 \\ C(y, 0) &= 0, & C(-h, t) &= C_1, & C(h, t) &= C_2 \end{aligned} \right\} \quad (7)$$

Where ρ and μ are respectively the density and apparent viscosity of the fluid, σ is electric conductivity, β is Hall factor, Bi is ion slip parameter, $Be = \sigma\beta B_0$ is Hall parameter, c and k are respectively the specific heat capacity and thermal conductivity of the fluid. Where u and w are components of velocities along and perpendicular to the plate in x and y directions respectively, σ is the electrical conductivity, β_T is the coefficient of volume expansion of the moving fluid, β_C is the coefficient of volumetric expansion with concentration, ν is the kinematic viscosity, T is the temperature of the fluid, C is the concentration of the fluid, C_1 is concentration at infinity, D_1 the thermal diffusivity, D_2 the chemical reaction rate constant, C_p is the specific heat capacity at constant pressure. t is time, g is gravitational force, μ_e is magnetic permeability of the fluid, K is the porous media permeability coefficient, q is radiative heat flux, H_0 is intensity of magnetic field, $B_0 = \mu_e H_0$ is electromagnetic induction, τ_0 is yield stress, β is coefficient of volume expansion due to temperature and α is mean radiation absorption coefficient.

To write the governing dimensional equations (3)-(6) with their corresponding boundary conditions (7) in non-dimensional form, we use the following dimensionless variables:

Time Dependent Pressure Gradient Effects on Unsteady MHD Couette Flow Through a Parallel Porous Plate

$$\bar{u} = \frac{u}{U_0}, \quad \bar{w} = \frac{w}{U_0}, \quad \bar{y} = \frac{y}{h}, \quad \bar{x} = \frac{x}{h}, \quad \bar{t} = \frac{tU_0}{h}, \quad \theta = \frac{T - T_1}{T_2 - T_1} \tag{8}$$

$$\phi = \frac{C - C_1}{C_2 - C_1}, \quad \bar{P} = \frac{P}{\rho U_0^2}, \quad \bar{\mu} = \frac{c\mu_1 T}{T_1}$$

When the pressure gradient is a function of time: $\frac{\partial p}{\partial x} = \frac{dp}{dx} = -\lambda e^{-\epsilon t}$ (9)

In this case, equations (3) - (6) reduce to;

$$\frac{\partial u}{\partial t} + \frac{S}{2} \frac{\partial u}{\partial z} = -\lambda e^{-\epsilon t} + \frac{c}{4\text{Re}} \frac{\partial}{\partial z} \left((1 + \alpha\theta) \frac{\partial u}{\partial z} \right) - \frac{Ha^2}{\text{Re}((1 + BiBe)^2 + Be^2)} \left((1 + BiBe)^2 u + Be^2 w \right) -$$

$$\frac{cP}{\text{Re}} (\alpha\theta + 1)u + Gr_\theta\theta + Gr_\phi\phi$$

(10)

$$\frac{\partial w}{\partial t} + \frac{S}{2} \frac{\partial w}{\partial z} = \frac{c}{4\text{Re}} \frac{\partial}{\partial z} \left((1 + \alpha\theta) \frac{\partial w}{\partial z} \right) - \frac{Ha^2}{\text{Re}((1 + BiBe)^2 + Be^2)} \left((1 + BiBe)^2 w - Be^2 u \right) -$$

$$\frac{cP}{\text{Re}} (\alpha\theta + 1)w$$

(11)

$$\frac{\partial \theta}{\partial t} + \frac{S}{2} \frac{\partial \theta}{\partial z} = \frac{c}{4\text{Re Pr}} \frac{\partial}{\partial z} \left((1 + \alpha\theta) \frac{\partial \theta}{\partial z} \right) + \frac{cEc}{4\text{Re}} (1 + \alpha\theta) \left(\left(\frac{\partial u}{\partial z} \right)^2 + \left(\frac{\partial w}{\partial z} \right)^2 \right) +$$

$$\frac{EcHa^2}{\text{Re}((1 + BiBe)^2 + Be^2)} (u^2 + w^2) - Ra^2\theta$$

(12)

$$\frac{\partial \phi}{\partial t} + \frac{S}{2} \frac{\partial \phi}{\partial z} = \frac{c}{4Sc\text{Re}} \frac{\partial}{\partial z} \left((1 + \alpha\theta) \frac{\partial \phi}{\partial z} \right) + \frac{T_D}{4} \frac{\partial^2 \theta}{\partial z^2} - K_r\phi$$

(13)

Subject to the initial and boundary conditions

$$\left. \begin{aligned} u(y, 0) &= 0, & u(-1, t) &= 0, & u(1, t) &= 1 \\ w(y, 0) &= y(1 - y), & w(-1, t) &= 0, & w(1, t) &= 0 \\ \theta(y, 0) &= 0, & \theta(-1, t) &= 0, & \theta(1, t) &= 1 \\ \phi(y, 0) &= 0, & \phi(-1, t) &= 0, & \phi(1, t) &= 1 \end{aligned} \right\}$$

(14)

Where

Time Dependent Pressure Gradient Effects on Unsteady MHD Couette Flow Through a Parallel Porous Plate

$$\left. \begin{aligned} \text{Re} &= \frac{\rho U_0 h}{\mu_1}, & S &= \frac{v_0}{U_0}, & P &= \frac{h^2 \mu_1}{k}, & Ha^2 &= \frac{\sigma B_0^2 h^2}{\mu_1}, & Gr_\theta &= \frac{g \beta_T (T_2 - T_1) h}{\rho U_0^2}, \\ Gr_\phi &= \frac{g \beta_C (C_2 - C_1) h}{\rho U_0^2}, & \text{Pr} &= \frac{\mu_1 c_p}{k}, & Ec &= \frac{U_0^2}{c_p (T_2 - T_1)}, & Ra^2 &= \frac{4 \alpha^2 h}{\rho^2 C_p^2 U_0}, \\ Sc &= \frac{U_0 h}{D}, & T_D &= \frac{D (T_2 - T_1)}{h (C_2 - C_1) U_0}, & a &= \frac{T_2 - T_1}{T_1}, & Kr &= \frac{D_2 h}{\rho U_0}, \end{aligned} \right\}$$

METHOD OF SOLUTION

Since the boundary conditions are from -1 to 1, we first transform the boundary conditions to 0 to 1 using the transformation:

$$z = \frac{y+1}{2} \quad (15)$$

Let $0 < S \ll 1$ and $Ec = bS$, $a = eS$, $Be = fS$, $Gr_\theta = gS$, $Gr_\phi = hS$ such that

$$\left. \begin{aligned} u(z, t) &= u_0(z, t) + Su_1(z, t) + \dots \\ w(z, t) &= w_0(z, t) + Sw_1(z, t) + \dots \\ \theta(z, t) &= \theta_0(z, t) + S\theta_1(z, t) + \dots \\ \phi(z, t) &= \phi_0(z, t) + S\phi_1(z, t) + \dots \end{aligned} \right\} \quad (16)$$

Collecting like powers of S, we have for:

$$\left. \begin{aligned} S^0: \\ \frac{\partial \theta_0}{\partial t} &= \frac{c}{4 \text{Re Pr}} \frac{\partial}{\partial z} \left[\frac{\partial \theta_0}{\partial z} \right] - Ra^2 \theta_0 \\ \theta_0(z, 0) &= 0, \quad \theta_0(0, t) = 0, \quad \theta_0(1, t) = 1 \end{aligned} \right\} \quad (17)$$

$$\left. \begin{aligned} \frac{\partial \phi_0}{\partial t} &= \frac{c}{4Sc \text{Re}} \frac{\partial}{\partial z} \left[\frac{\partial \phi_0}{\partial z} \right] + T_D \frac{\partial^2 \theta_0}{\partial z^2} - Kr \phi_0 \\ \phi_0(z, 0) &= 0, \quad \phi_0(0, t) = 0, \quad \phi_0(1, t) = 1 \end{aligned} \right\} \quad (18)$$

$$\left. \begin{aligned} \frac{\partial w_0}{\partial t} &= \frac{c}{4 \text{Re}} \frac{\partial}{\partial z} \left(\frac{\partial w_0}{\partial z} \right) - \frac{Ha^2}{\text{Re}} [w_0] - \frac{Pc}{\text{Re}} [w_0] \\ w_0(z, 0) &= (2z-1)(2-2z), \quad w_0(0, t) = 0, \quad w_0(1, t) = 0 \end{aligned} \right\} \quad (19)$$

$$\left. \begin{aligned} \frac{\partial u_0}{\partial t} &= \frac{c}{4\text{Re}} \frac{\partial}{\partial z} \left(\frac{\partial u_0}{\partial z} \right) - \frac{Ha^2}{\text{Re}} [u_0] - \frac{Pc}{\text{Re}} (u_0) + \sigma \\ u_0(z, 0) &= 0, \quad u_0(0, t) = 0, \quad u_0(1, t) = 1 \end{aligned} \right\} \quad (20)$$

S^{-1} :

$$\left. \begin{aligned} \frac{\partial u_1}{\partial t} + \frac{1}{2} \frac{\partial u_0}{\partial z} &= \frac{c}{4\text{Re}} \frac{\partial}{\partial z} \left(\frac{e\theta_0 \partial u_0}{\partial z} + \frac{\partial u_1}{\partial z} \right) - \frac{Ha^2}{\text{Re}} [u_0 Bif + u_1 + fw_0] - \frac{Pc}{\text{Re}} (e\theta_0 u_0 + u_1) + \\ g\theta_0 + h\phi_0 \\ u_1(z, 0) &= 0, \quad u_1(0, t) = 0, \quad u_1(1, t) = 0 \end{aligned} \right\} \quad (21)$$

$$\left. \begin{aligned} \frac{\partial \theta_1}{\partial t} + \frac{1}{2} \frac{\partial \theta_0}{\partial z} &= \frac{c}{4\text{RePr}} \frac{\partial}{\partial y} \left[e\theta_0 \frac{\partial \theta_0}{\partial z} + \frac{\partial \theta_1}{\partial z} \right] + \frac{bc}{4\text{Re}} \left[\left(\frac{\partial u_0}{\partial y} \right)^2 + \left(\frac{\partial w_0}{\partial y} \right)^2 \right] - \\ \frac{bHa^2}{\text{Re}} [(u_0)^2 + (w_0)^2] - Ra^2 \theta_1 \\ \theta_1(z, 0) &= 0, \quad \theta_1(0, t) = 0, \quad \theta_1(1, t) = 0 \end{aligned} \right\} \quad (22)$$

$$\left. \begin{aligned} \frac{\partial w_1}{\partial t} + \frac{1}{2} \frac{\partial w_0}{\partial z} &= \frac{c}{4\text{Re}} \frac{\partial}{\partial z} \left(e\theta_0 \frac{\partial w_0}{\partial z} + \frac{\partial w_1}{\partial z} \right) - \frac{Ha^2}{\text{Re}} [w_0 Bif + w_1 - fu_0] - \frac{Pc}{\text{Re}} (e\theta_0 w_0 + w_1) \\ w_1(z, 0) &= 0, \quad w_1(0, t) = 0, \quad w_1(1, t) = 0 \end{aligned} \right\} \quad (23)$$

$$\left. \begin{aligned} \frac{\partial \phi_1}{\partial t} + \frac{1}{2} \frac{\partial \phi_0}{\partial z} &= \frac{c}{4Sc\text{Re}} \frac{\partial}{\partial z} \left[e\theta_0 \frac{\partial \phi_0}{\partial z} + \frac{\partial \phi_1}{\partial z} \right] + T_D \frac{\partial^2 \theta_1}{\partial z^2} - Kr\phi_1 \\ \phi_1(z, 0) &= 0, \quad \phi_1(0, t) = 0, \quad \phi_1(1, t) = 0 \end{aligned} \right\} \quad (24)$$

EIGENFUNCTION EXPANSION TECHNIQUE

Now, consider the problem (see Myint-U and Debnath, (1987))

Time Dependent Pressure Gradient Effects on Unsteady MHD Couette Flow Through a Parallel Porous Plate

$$\left. \begin{aligned} \frac{\partial u}{\partial t} &= k \frac{\partial^2 u}{\partial x^2} + \alpha u + F(x, t) \\ u(x, 0) &= f(x), \quad u(0, t) = 0, \quad u(L, t) = 0 \end{aligned} \right\} \quad (25)$$

For the solution of problem (24), we assume a solution of the form

$$u(x, t) = \sum_{n=1}^{\infty} u_n(t) \sin \frac{n\pi}{L} x \quad (26)$$

Where

$$u_n(t) = \int_0^t e^{\left(\alpha - k\left(\frac{n\pi}{L}\right)^2\right)(t-\tau)} F_n(\tau) d\tau + b_n e^{\left(\alpha - k\left(\frac{n\pi}{L}\right)^2\right)t} \quad (27)$$

$$F_n(t) = \frac{2}{L} \int_0^L F(x, t) \sin \frac{n\pi}{L} x dx \quad (28)$$

$$b_n(t) = \frac{2}{L} \int_0^L F(x) \sin \frac{n\pi}{L} x dx \quad (29)$$

Comparing equation (17) – (24) with the (25) we obtain the solutions to the velocity (primary and secondary), temperature, and concentration distributions as

$$\theta_0(z, t) = z + \sum_{n=1}^{\infty} q_{11} (1 - e^{-q_{0t}}) \sin n\pi z \quad (30)$$

$$\phi_0(z, t) = z + v_2(z, t) \quad (31)$$

$$w_0(z, t) = \sum_{n=1}^{\infty} q_{10} e^{-q_{11}t} \text{Sinn}\pi z \quad (32)$$

$$u_0(z, t) = z + \sum_{n=1}^{\infty} \frac{q_{12}}{q_{11}} (1 - e^{-q_{11}t}) \text{Sinn}\pi z \quad (33)$$

$$u_1(z, t) = \sum_{n=1}^{\infty} u_5(t) \text{Sinn}\pi z \quad (34)$$

Where

$$\begin{aligned}
 u_5(t) &= q_{16} \left(\frac{1}{q_{11}} (1 - e^{-q_{11}t}) \right) + \sum_{n=1}^{\infty} q_{27} P_4 \left(\frac{1}{q_{11}} (1 - e^{-q_{11}t}) - te^{-q_{11}t} \right) + \\
 &\sum_{n=1}^{\infty} \sum_{n=1}^{\infty} q_{28} q_1 P_4 \left(\frac{1}{q_{11}} (1 - e^{-q_{11}t}) - te^{-q_{11}t} - \frac{1}{q_{11} - q_0} (e^{-q_0t} - e^{-q_{11}t}) - \frac{1}{q_0} (e^{(q_{11}-q_0)t} - e^{-q_{11}t}) \right) + \\
 &\sum_{n=1}^{\infty} q_{29} q_1 \left(\frac{1}{q_{11}} (1 - e^{-q_{11}t}) - \frac{1}{q_{11} - q_0} (e^{-q_0t} - e^{-q_{11}t}) \right) + \\
 &\left(\sum_{n=1}^{\infty} q_4 \left(\frac{1}{q_{11}} (1 - e^{-q_{11}t}) - \frac{1}{q_{11} - q_2} (e^{-q_2t} - e^{-q_{11}t}) \right) + \right. \\
 &q_{26} \left. \sum_{n=1}^{\infty} \sum_{n=1}^{\infty} q_5 P_1 \left(\frac{1}{q_{11}} (1 - e^{-q_{11}t}) - te^{-q_{11}t} - \frac{1}{q_{11} - q_2} (e^{-q_2t} - e^{-q_{11}t}) \right) - \right. \\
 &\left. \sum_{n=1}^{\infty} \sum_{n=1}^{\infty} q_5 P_2 \left(\frac{1}{q_{11} - q_0} (e^{-q_0t} - e^{-q_{11}t}) - \frac{1}{q_{11} - q_2} (e^{-q_2t} - e^{-q_{11}t}) \right) \right) \\
 \theta_1(z, t) &= \sum_{n=1}^{\infty} u_6(t) \text{Sinn}\pi z \tag{35}
 \end{aligned}$$

Where

$$\begin{aligned}
 u_6(t) &= \left(\sum_{n=1}^{\infty} q_1 q_{30} \left(\frac{1}{q_0} (1 - e^{-q_0t}) - te^{-q_0t} \right) + \sum_{n=1}^{\infty} \sum_{n=1}^{\infty} q_1^2 q_{31} \left(\frac{1}{q_0} (1 - e^{-q_0t}) - 2te^{-q_0t} - \frac{1}{q_0} (e^{-2q_0t} - e^{-q_0t}) \right) \right) + \\
 &q_{32} \frac{1}{q_0} (1 - e^{-q_0t}) + \sum_{n=1}^{\infty} \sum_{n=1}^{\infty} q_{10}^2 q_{33} \left(\frac{1}{q_0 - 2q_{11}} (e^{-2q_{11}t} - e^{-q_0t}) \right) + \\
 &\sum_{n=1}^{\infty} q_{34} P_4 \left(\frac{1}{q_0} (1 - e^{-q_0t}) - \frac{1}{q_0 - q_{11}} (e^{-q_{11}t} - e^{-q_0t}) \right) + \\
 &\sum_{n=1}^{\infty} \sum_{n=1}^{\infty} q_{35} P_4^2 \left(\frac{1}{q_0} (1 - e^{-q_0t}) - \frac{2}{q_0 - q_{11}} (e^{-q_{11}t} - e^{-q_0t}) + \frac{1}{q_0 - 2q_{11}} (e^{-2q_{11}t} - e^{-q_0t}) \right) \\
 w_1(z, t) &= \sum_{n=1}^{\infty} u_7(t) \text{Sinn}\pi z \tag{36}
 \end{aligned}$$

Where

$$\begin{aligned}
 u_7(t) &= \left(q_{10} q_{36} (te^{-q_{11}t}) + \sum_{n=1}^{\infty} \sum_{n=1}^{\infty} q_{37} q_1 q_{10} \left(te^{-q_{11}t} + \frac{1}{q_0} (e^{-(q_{11}-q_0)t} - e^{-q_{11}t}) \right) + q_{38} \left(\frac{1}{q_{11}} (1 - e^{-q_{11}t}) \right) \right) + \\
 &\sum_{n=1}^{\infty} q_{14} P_4 \left(\frac{1}{q_{11}} (1 - e^{-q_{11}t}) + te^{-q_{11}t} \right)
 \end{aligned}$$

$$\phi_1(z, t) = \sum_{n=1}^{\infty} u_8(t) \text{Sinn}\pi z \tag{37}$$

Where

$$u_8(t) = \left(\begin{aligned} & \left(\sum_{n=1}^{\infty} \sum_{n=1}^{\infty} q_{43} \frac{(1 - e^{-q_2 t})}{q_2} - \sum_{n=1}^{\infty} \sum_{n=1}^{\infty} q_{44} \frac{(e^{-q_0 t} - e^{-q_2 t})}{q_2 - q_0} - \right. \\ & \sum_{n=1}^{\infty} \sum_{n=1}^{\infty} q_{45} \frac{t(e^{-q_0 t} - e^{-q_2 t})}{q_2 - q_0} + \sum_{n=1}^{\infty} \sum_{n=1}^{\infty} \sum_{n=1}^{\infty} q_{46} \frac{(1 - e^{-q_2 t})}{q_2} - \sum_{n=1}^{\infty} \sum_{n=1}^{\infty} \sum_{n=1}^{\infty} q_{47} \frac{(e^{-q_0 t} - e^{-q_2 t})}{q_2 - q_0} - \\ & 2 \sum_{n=1}^{\infty} \sum_{n=1}^{\infty} \sum_{n=1}^{\infty} q_{48} \frac{t(e^{-q_0 t} - e^{-q_2 t})}{q_2 - q_0} - \sum_{n=1}^{\infty} \sum_{n=1}^{\infty} \sum_{n=1}^{\infty} q_{49} \frac{(e^{-q_0 t} - e^{-q_2 t})}{q_2 - q_0} + \sum_{n=1}^{\infty} \sum_{n=1}^{\infty} \sum_{n=1}^{\infty} q_{50} \frac{(e^{-q_0 t} - e^{-q_2 t})}{q_2 - q_0} + \\ & q_{39} \sum_{n=1}^{\infty} q_{51} \left(\frac{(1 - e^{-q_2 t})}{q_2} - \frac{(e^{-q_0 t} - e^{-q_2 t})}{q_2 - q_0} \right) + \sum_{n=1}^{\infty} \sum_{n=1}^{\infty} \sum_{n=1}^{\infty} q_{52} \frac{(e^{-2q_{11} t} - e^{-q_2 t})}{q_2 - q_0} - \sum_{n=1}^{\infty} \sum_{n=1}^{\infty} \sum_{n=1}^{\infty} q_{53} \frac{(e^{-2q_{11} t} - e^{-q_2 t})}{q_2 - q_0} + \\ & \sum_{n=1}^{\infty} \sum_{n=1}^{\infty} q_{54} \frac{(1 - e^{-q_2 t})}{q_2} - \sum_{n=1}^{\infty} \sum_{n=1}^{\infty} q_{55} \frac{(e^{-q_0 t} - e^{-q_2 t})}{q_2 - q_0} - \sum_{n=1}^{\infty} \sum_{n=1}^{\infty} q_{56} \frac{(e^{-q_{11} t} - e^{-q_2 t})}{q_2 - q_{11}} + \sum_{n=1}^{\infty} \sum_{n=1}^{\infty} q_{57} \frac{(e^{-q_0 t} - e^{-q_2 t})}{q_2 - q_0} + \\ & \sum_{n=1}^{\infty} \sum_{n=1}^{\infty} \sum_{n=1}^{\infty} q_{58} \left(\frac{(1 - e^{-q_2 t})}{q_2} - \frac{(e^{-q_0 t} - e^{-q_2 t})}{q_2 - q_0} \right) - 2 \sum_{n=1}^{\infty} \sum_{n=1}^{\infty} \sum_{n=1}^{\infty} q_{59} \frac{(e^{-q_{11} t} - e^{-q_2 t})}{q_2 - q_{11}} + 2 \sum_{n=1}^{\infty} \sum_{n=1}^{\infty} \sum_{n=1}^{\infty} q_{60} \frac{(e^{-q_0 t} - e^{-q_2 t})}{q_2 - q_0} + \\ & \left. \sum_{n=1}^{\infty} \sum_{n=1}^{\infty} \sum_{n=1}^{\infty} q_{61} \frac{(e^{-2q_{11} t} - e^{-q_2 t})}{q_2 - 2q_{11}} + \sum_{n=1}^{\infty} \sum_{n=1}^{\infty} \sum_{n=1}^{\infty} q_{62} \frac{(e^{-q_0 t} - e^{-q_2 t})}{q_2 - q_0} \right) \\ & q_{40} \frac{(1 - e^{-q_2 t})}{q_2} + \\ & q_{41} \left(- \sum_{n=1}^{\infty} q_4 \frac{(1 - e^{-q_2 t})}{q_2} + \sum_{n=1}^{\infty} q_4 t e^{-q_2 t} + \sum_{n=1}^{\infty} \sum_{n=1}^{\infty} q_5 P_1 \frac{(1 - e^{-q_2 t})}{q_2} - \sum_{n=1}^{\infty} \sum_{n=1}^{\infty} q_5 P_1 t e^{-q_2 t} - \sum_{n=1}^{\infty} \sum_{n=1}^{\infty} q_5 P_2 \frac{(e^{-q_0 t} - e^{-q_2 t})}{q_2 - q_0} \right) \\ & \sum_{n=1}^{\infty} \sum_{n=1}^{\infty} q_5 P_2 t e^{-q_2 t} \\ & q_{42} \left(- \sum_{n=1}^{\infty} \sum_{n=1}^{\infty} q_1 q_4 \left(\frac{(1 - e^{-q_2 t})}{q_2} - t e^{-q_2 t} \right) + \sum_{n=1}^{\infty} \sum_{n=1}^{\infty} q_5 q_1 P_1 \left(\frac{(1 - e^{-q_2 t})}{q_2} - t e^{-q_2 t} \right) - \sum_{n=1}^{\infty} \sum_{n=1}^{\infty} q_5 q_1 P_2 \left(\frac{(e^{-q_0 t} - e^{-q_2 t})}{q_2 - q_0} - t e^{-q_2 t} \right) + \right. \\ & \sum_{n=1}^{\infty} \sum_{n=1}^{\infty} q_1 q_4 \left(\frac{(e^{-q_0 t} - e^{-q_2 t})}{q_2 - q_0} - \frac{(e^{-(q_2 + q_0)t} - e^{-q_2 t})}{q_0} \right) + \sum_{n=1}^{\infty} \sum_{n=1}^{\infty} \sum_{n=1}^{\infty} q_5 q_1 P_1 \left(\frac{(e^{-q_0 t} - e^{-q_2 t})}{q_2 - q_0} - \frac{(e^{-(q_2 + q_0)t} - e^{-q_2 t})}{q_0} \right) + \\ & \left. \sum_{n=1}^{\infty} \sum_{n=1}^{\infty} \sum_{n=1}^{\infty} q_5 q_1 P_2 \left(\frac{(e^{-q_0 t} - e^{-q_2 t})}{q_2 - q_0} - \frac{(e^{-(q_2 + q_0)t} - e^{-q_2 t})}{q_0} \right) \right) \end{aligned} \right)$$

Therefore the solutions to the governing equations are given as:

$$\theta(z, t) = z + \sum_{n=1}^{\infty} q_1 (1 - e^{-q_0 t}) \sin n\pi z + \sum_{n=1}^{\infty} u_6(t) \text{Sinn}\pi z \tag{38}$$

$$\phi(z, t) = z + v_2(z, t) + s \sum_{n=1}^{\infty} u_8(t) \text{Sinn}\pi z \tag{39}$$

$$w(z, t) = \sum_{n=1}^{\infty} q_{10} e^{-q_{11}t} \text{Sinn}\pi z + s \sum_{n=1}^{\infty} u_7(t) \text{Sinn}\pi z \tag{40}$$

$$u(z, t) = z + \sum_{n=1}^{\infty} \frac{q_{12}}{q_{11}} (1 - e^{-q_{11}t}) \text{Sinn}\pi z + s \sum_{n=1}^{\infty} u_5(t) \text{Sinn}\pi z \tag{41}$$

4. RESULTS AND DISCUSSIONS

The system of partial differential equations describing unsteady couette flow of an electrically conducting incompressible fluid bounded by two parallel non conducting porous plates are solved analytically using eigenfunction expansion method. The analytical solutions of the governing equations are computed and presented graphically with the aid of a computer symbolic algebraic package MAPLE 17 for the values of the following parameters:

$$\begin{aligned} \text{Re} = 1, & \quad Ra^2 = 1, & \quad S = 0.1, & \quad \text{Pr} = 1 \\ Bi = 1, & \quad Be = 1, & \quad \alpha = 0.1, & \quad a = 0.2, \\ Gr_{\theta} = 0.2, & \quad Gr_{\phi} = 0.2, & \quad \sigma = 2 \end{aligned}$$

The figures 2-9 Explains the graphs of primary and secondary velocities, temperature and concentration against different dimensionless parameters.

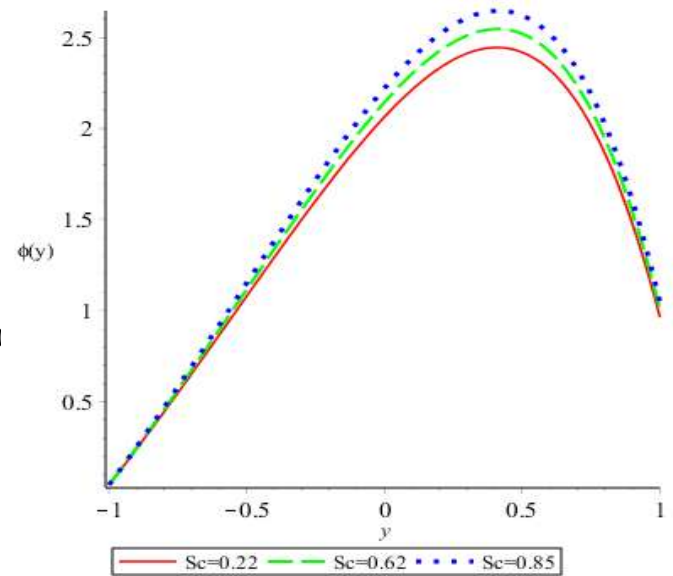


Figure 3: Effect of Schimidt number (*Sc*) on concentration profile $\phi(y, t)$

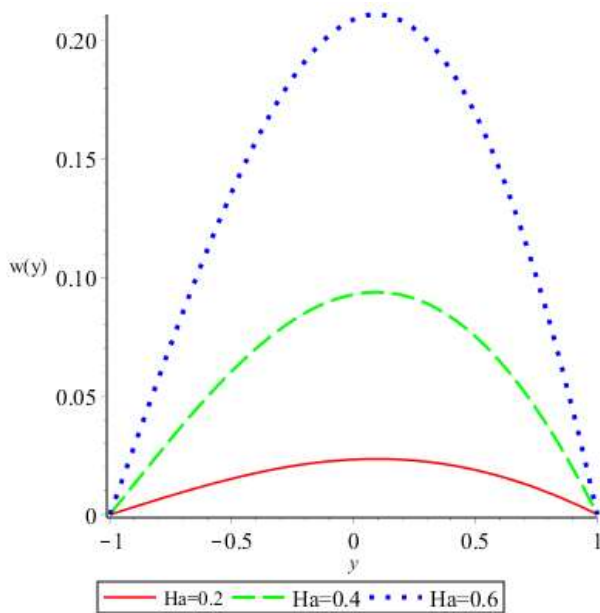


Figure 2: Effect of Hartman number (*Ha*) on secondary velocity profile $w(y, t)$

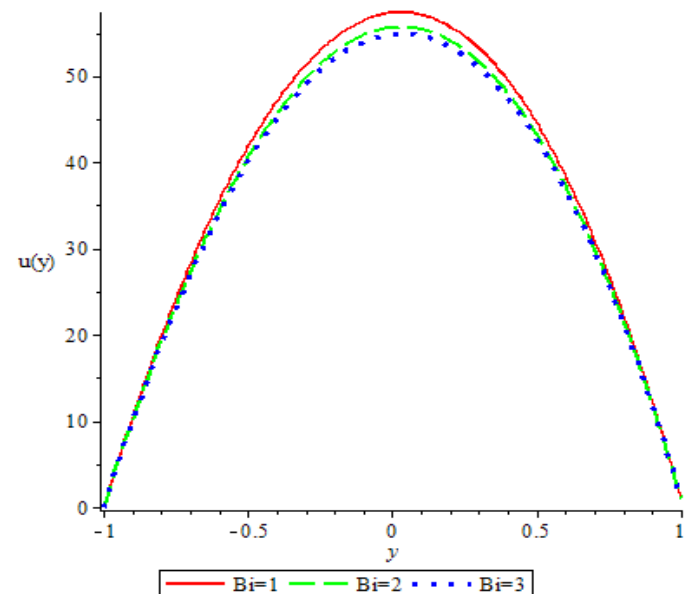


Figure 4: Effect of ion slip parameter (*Bi*) on primary velocity profile $u(y)$

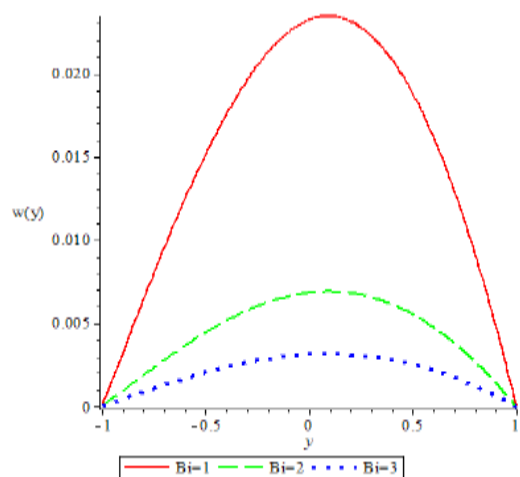


Figure 5: Effect of ion slip parameter (Bi) on secondary velocity profile $w(y)$

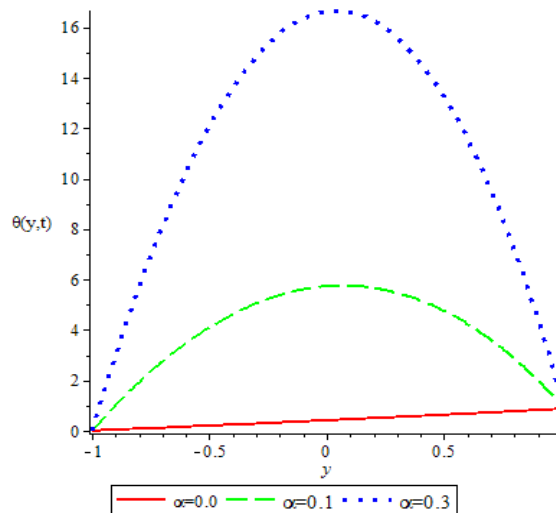


Figure 8: Effect of temperature dependent viscosity (α) on temperature profile $\theta(y)$

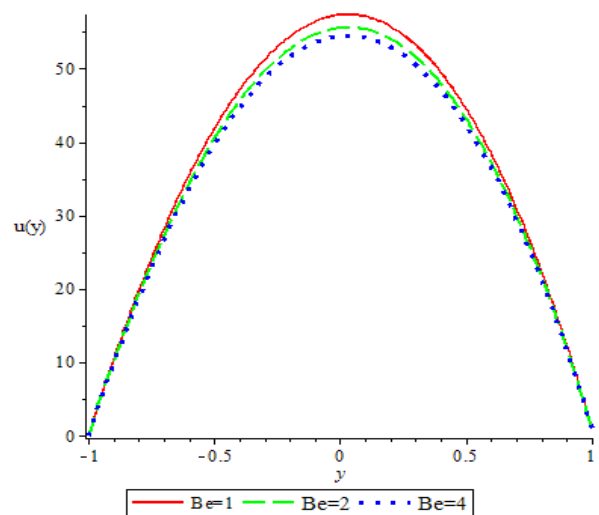


Figure 6: Effect of Hall parameter (Be) on primary velocity profile $u(y)$

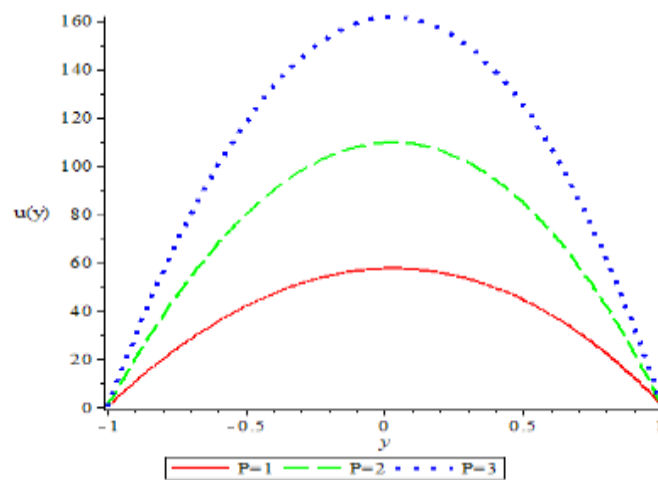


Figure 9: Effect of porosity parameter (P) on primary velocity profile $u(y)$

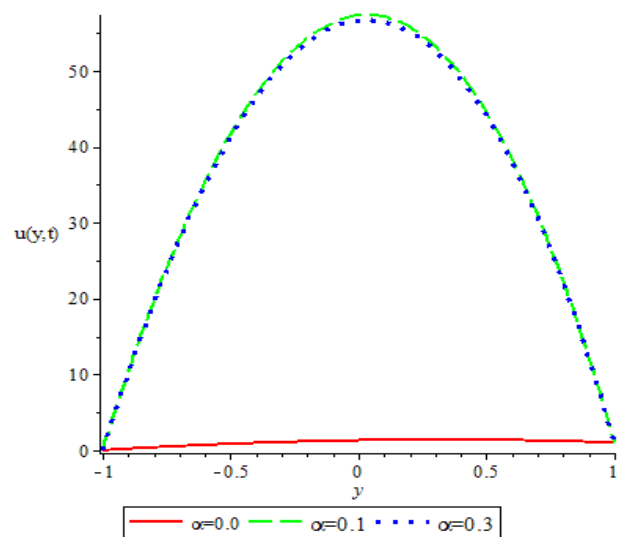


Figure 7: Effect of temperature dependent viscosity (α) on primary velocity profile $u(y)$

Figure 2 depicts the graph of secondary velocity for different values of Hartman number. It is observed that secondary velocity increases and then decreases along distance y . Also, increase in Hartman number leads to increase in secondary velocity.

Figure 3 depicts the graph of concentration for different values of Schmidt number. It is observed that concentration increases and then decreases along distance y . Also, increase in Schmidt number leads to increase in concentration.

Figure 4 depicts the graph of primary velocity for different values of Hall parameter. It is observed that primary velocity increases and then decreases along distance y . Also, increase in Hall parameter leads to decrease in primary velocity.

Figure 5 depicts the graph of secondary velocity for different values of Hall parameter. It is observed that secondary velocity increases and then decreases along distance y . Also, increase in Hall parameter leads to decrease in secondary velocity.

Figure 6 depicts the graph of primary velocity for different values of Hall factor. It is observed that primary velocity increases and then decreases along distance y . Also, increase in Hall decrease leads to decrease in primary velocity.

Figure 7 depicts the graph of primary velocity $u(y, t)$ for different values of temperature dependent viscosity (α). It is observed that primary velocity is maximum when viscosity is temperature dependent as compared to when it is independent on temperature. Also, increase in temperature dependent viscosity leads to oscillation in primary velocity along distance y .

Figure 8 depicts the graph of temperature profile $\theta(y, t)$ for different values of temperature dependent viscosity (α). It is observed that temperature increases with increase in viscosity. Also, increase in temperature dependent viscosity leads to increase in temperature along distance y .

Figure 9 shows the effect of porosity parameter on primary velocity profile along distance y . It is observed that the primary velocity increases and then decreases along y while increase in porosity parameter leads to increase in primary velocity.

5. Conclusion

For temperature dependent pressure gradient, the unsteady MHD Couette flow through a porous medium of a viscous incompressible fluid bounded by two parallel porous plates under the influence of thermal radiation and chemical reaction is investigated. A uniform suction and injection are applied perpendicular to the plate. The transformed conservation equations are solved analytically subject to physically appropriate boundary conditions by using Eigenfunction expansion technique. From the results obtained, we can conclude that:

1. It is observed that temperature increases with increase in viscosity. Also, increase in temperature dependent viscosity leads to increase in temperature along distance y .
2. Concentration profile increases with time and also, increases as Reynolds number increases.
3. Increase in the radiation parameter is found to decelerate the velocity of the flow.
4. The flow field suffers a decrease in temperature as radiation parameter increases while as radiation parameter the temperature profile is observed to decrease with time t .

Conflict of Interest

We wish to state that there are no conflict of interest since Anyanwu *et al.* [1] considered the model equation under constant pressure gradient while this study is considered under time dependent pressure gradient.

REFERENCES

1. E.O. Anyanwu, R.O. Olayiwola, M.D. Shehu and A.Lawal. Radiative Effects on Unsteady MHD Couette Flow through a Parallel Plate with Constant Pressure Gradient. *Asian Research Journal of Mathematics*. 2020; 16(9): 1-19.
2. Olayiwola R.O. Modelling and Simulation of Combustion Fronts in Porous Media. *Journal of the Nigerian Mathematical Society* 2015: 34, 1-10
3. Jana M, Das S, Jana RN. Unsteady Couette flow through a porous medium in a rotating system. *Open Journal of fluid dynamics*. 2012; 2: 149-158
4. Seth GS, Ansari MS and Nandkeolyar R. Effects of rotation and magnetic field on unsteady Couette flow in a porous channel. *Journal of applied fluid mechanics*. 2011; 4: 95-103.
5. Seth GS, Ansari MS and Nandkeolyar R. Unsteady hydromagnetic Couette flow within porous plates in a rotating system. *Advanced Applied Mathematical Science*. 2010; 3: 2919-2932.
6. Sharma PR, Yadav GR. Heat transfer through three dimensional Couette flow between a stationary porous plate bounded by porous medium and moving porous plates. *Ultra Sci. Phys. Sci.* 2005; 17(3): 351-360.
7. Sharma PR, Gaur YN, Sharma RP. Steady laminar flow and heat transfer of a non-Newtonian fluid through a straight horizontal porous channel in the presence of heat source. *Ind. J. Theo. Phys.* 2005; 53(1): 37-47.
8. Olayiwola RO, Ayeni RO. A Mathematical Model and Simulation of In-situ Combustion in Porous Media. *Journal of Nigerian Mathematical Physics* 2012; 21: 545-554.
9. Olayiwola RO. A Mathematical Model of Solid Fuel Arrhenius Combustion in a Fixed-Bed. *International Journal of Numerical Mathematics* 2011; 6: 214-233.
10. Bhattacharyya K, Hayat T, Alsaedi A. Analytic solution of Magneto hydrodynamic boundary layer flow of Casson fluid over a stretching/shrinking sheet with wall mass transfer. *Journal of Chinese Physics*. 2013; 8 Article ID 024702.
11. Mustafa M, Hayat T, Pop I and Aziz A. Unsteady boundary layer flow of a Casson fluid due to an impulsively started moving flat plate. *Heat Transfer –Asian Resc.* 2011; 40: 563-576.
12. Mukhopadhyay S, Bhattacharyya K, Layek GC. Steady boundary layer flow and heat transfer over a porous moving plate in the presence of thermal radiation. *International Journal of heat and Mass transfer*. 2011; 54: 2751-2757.
13. Makinde OD and Mhone PY. Heat transfer to MHD oscillatory flow in a channel filled with porous medium. *Rom. Journ. Phys.* 2005; 50: 931-938.

Time Dependent Pressure Gradient Effects on Unsteady MHD Couette Flow Through a Parallel Porous Plate

14. Malapati V, Polarapu P. Unsteady MHD Free Convective Heat and Mass Transfer in a Boundary Layer Flow Past a Vertical Peamable Plate with Thermal Radiation and Chemical Reaction. *Procedia Engineering* 2015; 127: 791-799.
15. Chamka AJ and Ahmed SE, unsteady MHD heat and mass transfer by mixed convection flow in the forward stagnation region of a rotating sphere at different wall conditions, *Chemical Engineering Communications* 2012; 199: 122-141
16. Elbashbeshy EMA and Aldawody DA. The effects of thermal radiation and magnetic field on unsteady mixed convection flow and heat transfer over a stretching in the presence of internal heat generation/absorbtion *Int. J. Phy. Sci.* 2011; 6: 1540-1548.
17. Dulal Pal, Bulal Pal Talukdar. The bouancy and chemical reaction effects on MHD mixed convection heat and mass transfer in a porous medium with thermal radiation and ohmic heating, *Commun. Nonlinear Sci.Numer Simulat*, 2010; 15: 2878-2893.
18. Mohammed I, Gangadhar S. and Bhaskar RN. Radiation and mass transfer effects on MHD oscillatory flow in a channel filled with porous medium in the presence of chemical reaction. *Journal of Applied Fluid Mechanics* 2015; 8: 529-537.